Evolution of a High Performing, Modular Platform for AAV Manufacturing

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MEIRAGT_X

Introduction

MeiraGTx is continuously developing its adeno-associated viral (AAV) vector manufacturing platform upstream to maximize yield and minimize the generation of non-therapeutic AAV particles and other process-related contaminants.

work presented here shows the The MeiraGTx's evolution of upstream manufacturing platform.

AAV5

Size ITR-ITR: 4159 bp

AAV2

Size ITR-ITR: 4546 bp

AAV8

Size ITR-ITR: 3972 bp

Plasmids **Transfection** Reagent + () ()

DNA/TR

Polyplex

HEK293

Cell

Production



Methods

AAV

General

Suspension HEK293 cells were cultured in 250mL STRs to 2.0-3.5x10⁶ VC/mL and triple-transfected with two commercially available transfection reagents, with or without AAV production enhancers, to generate AAV5, AAV2, and AAV8. Product was harvested 3 to 4 days post-TFX. Harvest culture was clarified and purified via affinity chromatography (AAVX). Viral genome (VG) titre and residual pDNA (KanR) were determined in lysate using qPCR. % full capsids and hcDNA were

Partial **Full and** Residual hcDNA \leq 16 ng/ 10¹² VG with **Transfection Reagent A**

U

Lysate

Residual hcDNA \leq 31 ng/ 10¹² VG with Transfection Reagent B + Enhancer 2



• Residual hcDNA ≤ 8 ng/ 10¹² VG

• Residual hcDNA < 5 ng/ 10¹² VG

- All residual pDNA < 6% (KanR qPCR).
- Harvest VG titre > 5x10¹¹ VG/mL across multiple AAV serotypes.
- Use of Enhancer 2 resulted in a 1.4 to 5.2-fold increase in VG titre and comparable or improved % full capsids compared to No Enhancer.
- Enhancer 2 is currently the enhancer of choice for the fed-batch platform.

Perfusion-Enhanced HEK293 Triple-Transfection Platform

measured in AAVX eluate by AUC and qPCR, respectively.

Perfusion Culture

For cultures ran in perfusion mode, cells were recirculated through a hollow fibre filter at constant flow rate using a centrifugal pump (Levitronix, Switzerland). A total of 2 vessel volumes of medium was perfused over ~10h prior to transfection. HEK293 cells were transfected at a target VCD range of 4.5-5.0x10⁶ VC/mL.

Conclusions

- A modular upstream manufacturing process was developed and optimized internally at MeiraGTx, using different commercially available transfection reagents, AAV production enhancers, and finely-tuned transfection parameters.
- Fed-batch process optimization resulted in harvest AAV titres of up to **1.3x10¹² VG/mL** and up to **50% full**



capsids prior to polishing steps, for multiple combinations of serotype and therapeutic DNA cassette.

- Residual DNA levels were demonstrated to be controllable and adequate for patient safety.
- Enhancing the platform process using an optimized perfusion method has resulted in up to a **2.2X increase in** harvest VG titre, reaching 4.4x10¹² **VG/mL**, without compromising on product quality, whilst reducing pDNA usage by up to 50% and COGs per dose by 2.2-fold.



- pDNA usage was decreased by 33% to 50% and cost of goods (COGs) per dose was reduced by up to 2.2-fold.
- Residual hcDNA was reduced 1.4 to 2.4-fold versus fed-batch.
- All conditions showed residual pDNA \leq 4%.